# Section 9
# Steam System Optimization
# Condensate Recovery

Types of Steam Traps

Steam Trap Management Program

SSAT Evaluations & Economic Impacts

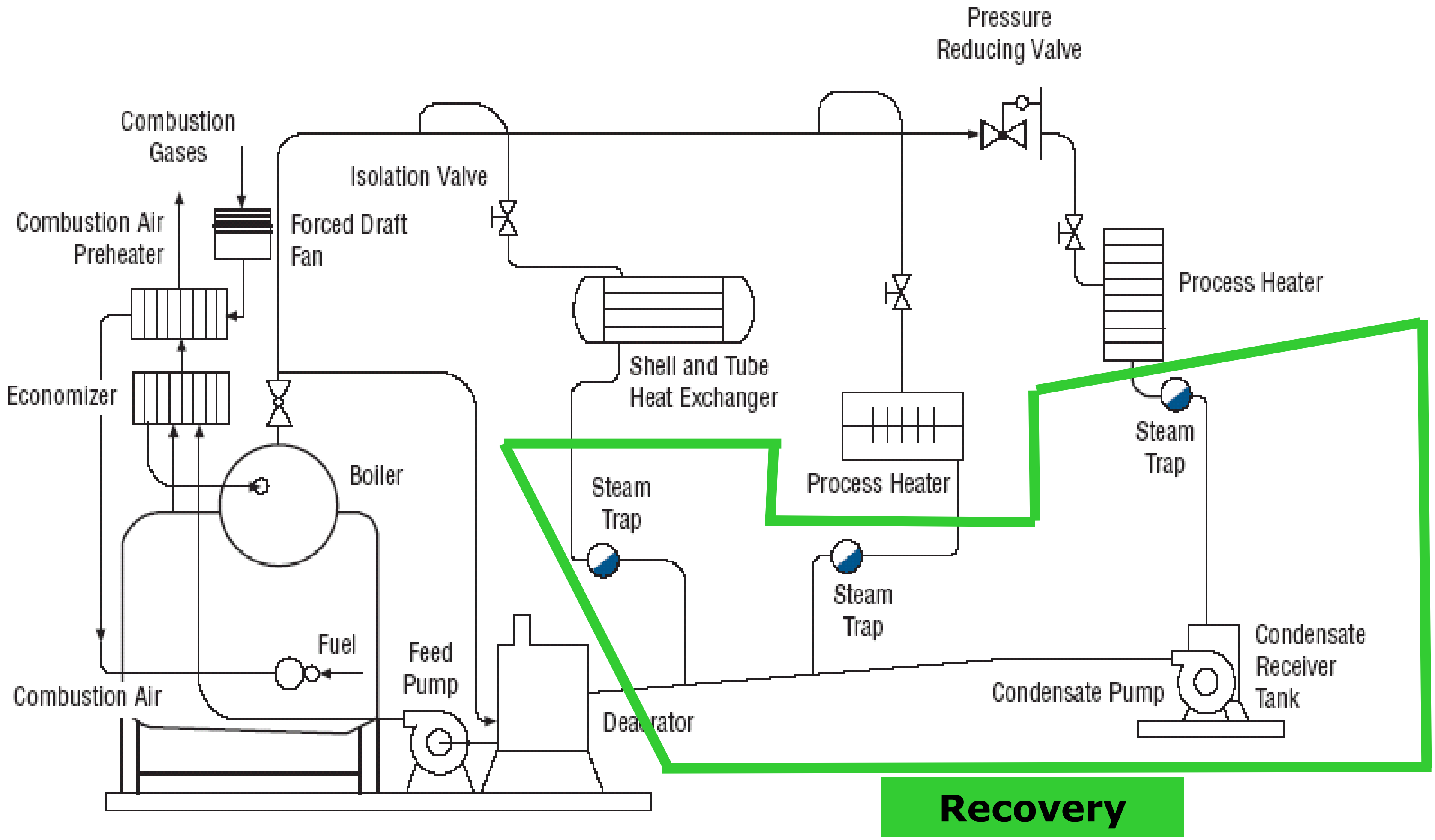
Evaluation of Condensate Recovery Systems

Condensate Flash Tanks

Condensate Tank Vents

SSAT Evaluations & Economic Impacts

# Generic Steam System




Source: US DOE ITP Steam BestPractices Program

# Steam Traps

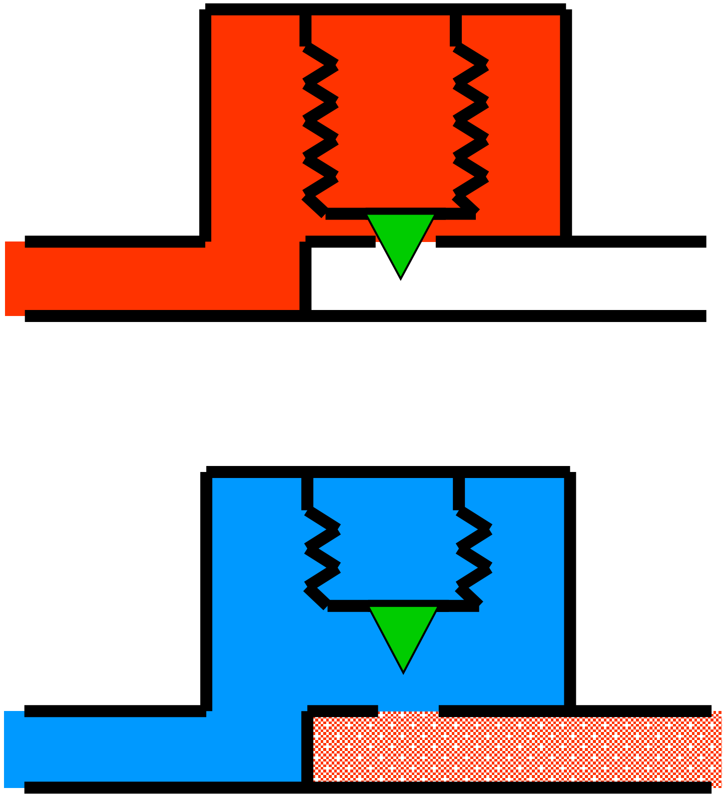
- ✓ Traps serve several vital operating functions for a steam system
  - During start-up, they allow air and large quantities of condensate to escape
  - During normal operation, they allow collected condensate to pass into the condensate return system, while minimizing (or eliminating) loss of steam
- ✓ There are different kinds of steam traps and hence, functionality and principles of operation must be understood
- ✓ All plants should have an effective steam trap management program
- ✓ Steam trap failures may not result in energy loss per se, but they will surely result in system operation problems and reliability issues

# Types of Steam Traps

- ✓ Thermostatic Traps
  - Bellows*
  - Bimetallic*
- ✓ Mechanical Traps
  - Ball Float
  - Float and Lever
  - Inverted Bucket*
  - Open Bucket
  - Float and Thermostatic*
- ✓ Thermodynamic Traps
  - Disc*
  - Piston
  - Lever
- ✓ Orifice Traps
  - Orifice Plate
  - Venturi Tube

* - Most commonly used

# Thermostatic Steam Traps

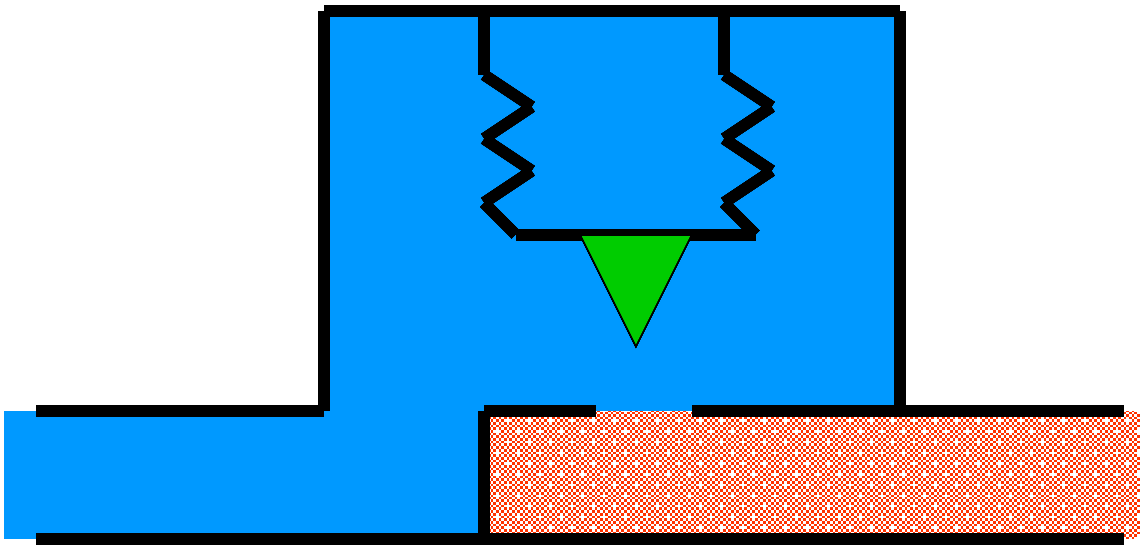


- ✓ Responds to temperature changes
- ✓ A bellows (with a volatile fluid) or a bimetallic strip closes the valve with high temperature steam
- ✓ When condensate (typically, sub-cooled) collects – the bellows contracts and opens the valve to let condensate drain out

Source: US DOE ITP Steam BestPractices Program

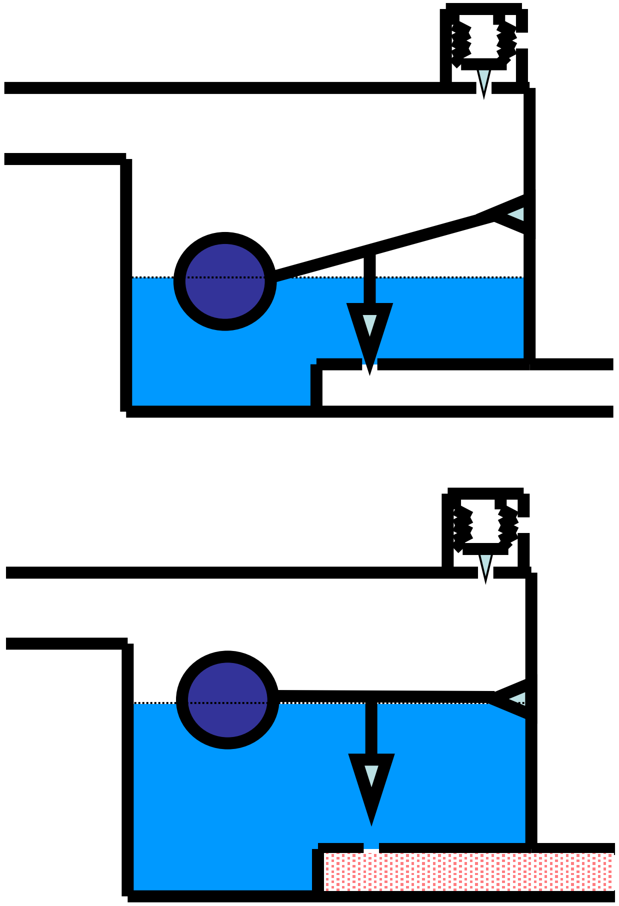
# Thermostatic Steam Traps

- ✓ Opens to subcooled condensate
- ✓ Depending on subcooling can discharge condensate or condensate and flash steam
- ✓ Allows energy recovery from condensate
- ✓ Significant air removal capability



Source: US DOE ITP Steam BestPractices Program

# Mechanical Steam Traps

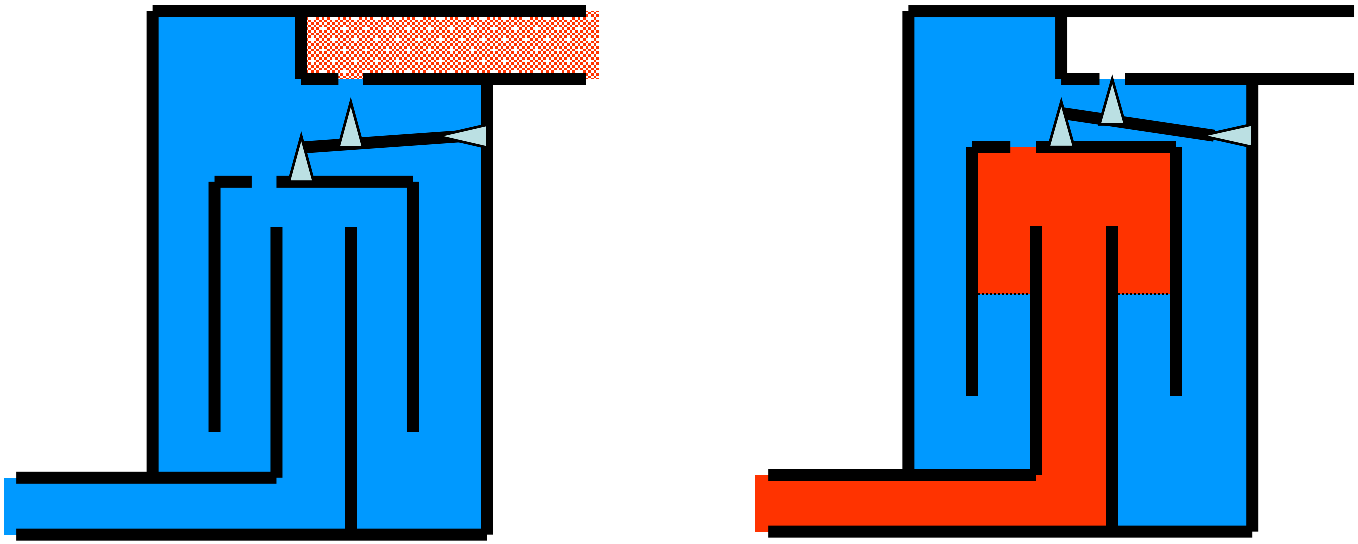


- ✓ Opens to saturated and/or sub-cooled condensate
- ✓ Will discharge condensate and flash steam
- ✓ Significant air removal and startup capabilities
- ✓ Modulating type operation

**Float & Thermostatic Trap (F&T)**

**Source: US DOE ITP Steam BestPractices Program**

# Mechanical Steam Traps

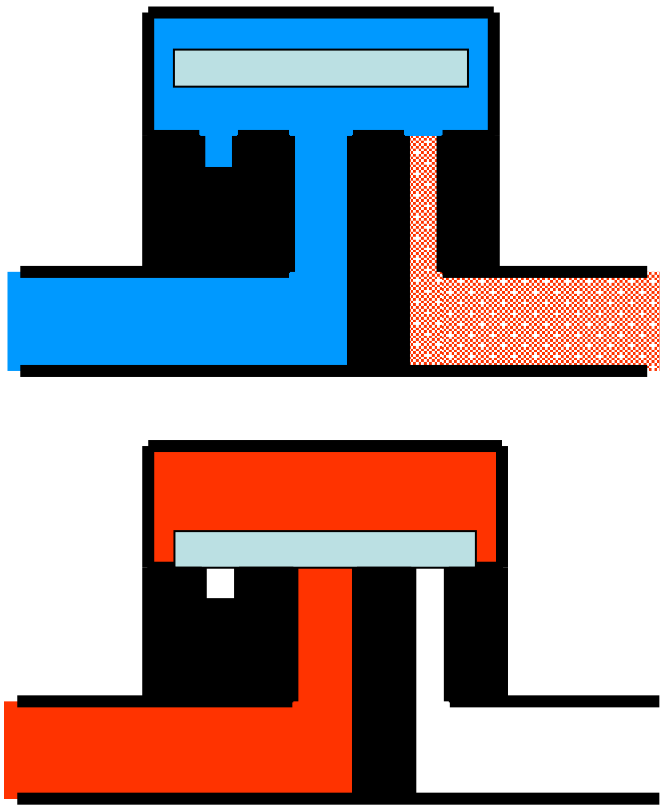


**Inverted Bucket Trap (Open Float)**

- Opens to saturated and/or sub-cooled condensate
- Will discharge condensate and flash steam
- Limited air removal and startup capabilities
- Application in superheated steam service should be questioned
- Intermittent operation

**Source: US DOE ITP Steam BestPractices Program**

# Thermodynamic Steam Traps

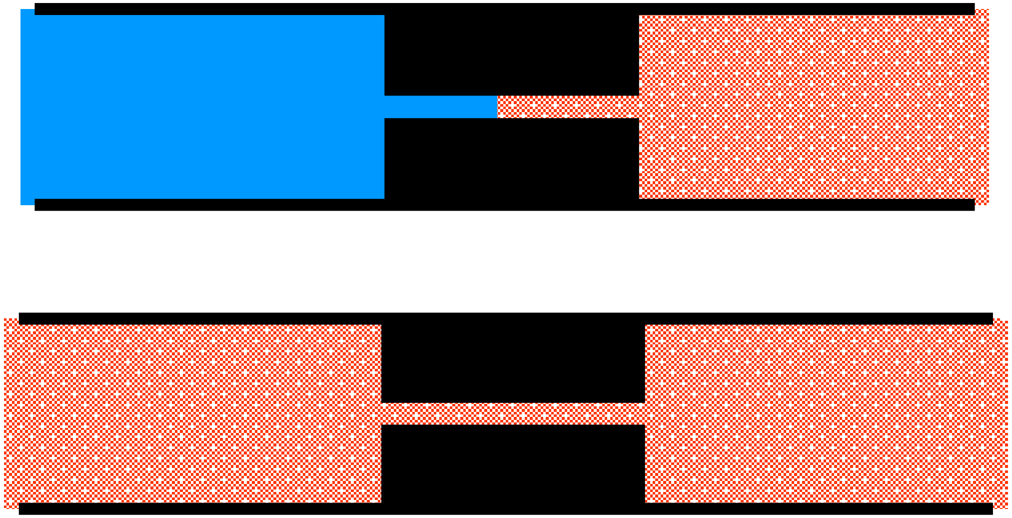


**Disc Trap**

- ✓ Works on the difference in kinetic energy (velocity) between condensate and steam to operate a valve
- ✓ Opens to saturated condensate
- ✓ Will discharge condensate and flash steam
- ✓ Intermittent operation
- ✓ Can be equipped with thermostatic element to improve air removal

**Source: US DOE ITP Steam BestPractices Program**

# Orifice Steam Traps

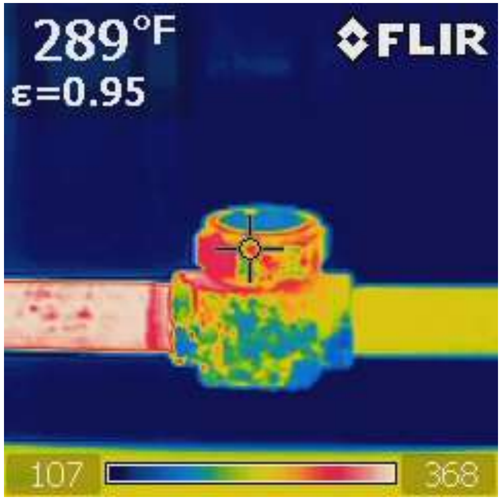


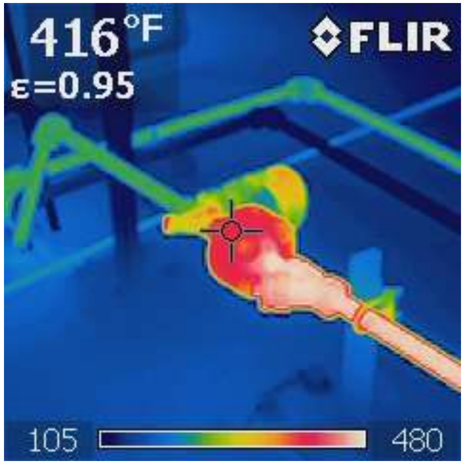
- No moving parts
- Continuous operation
- Common applications are steady loads
- Limited air removal capability due to orifice limitations

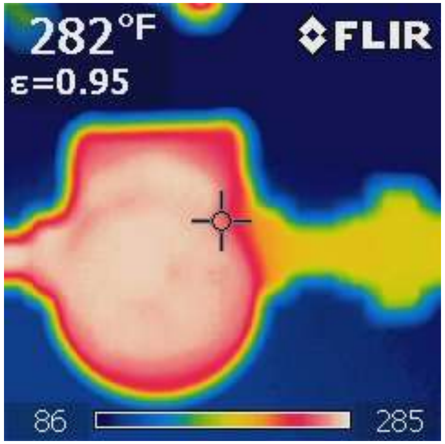
- Its designed for a specific amount of condensate removal
- If there is no condensate, then a small amount of steam leaks continuously

Source: US DOE ITP Steam BestPractices Program

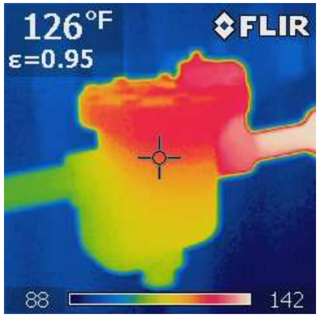
# Steam Traps in the Field

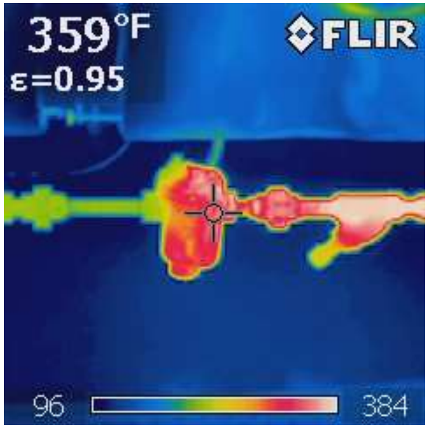


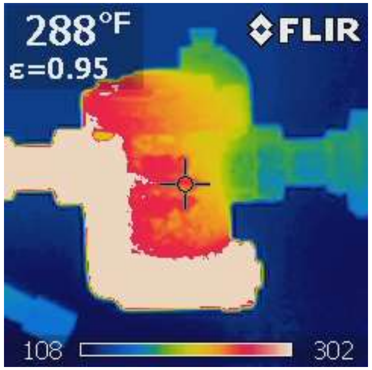



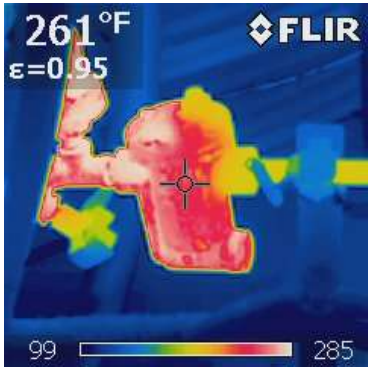



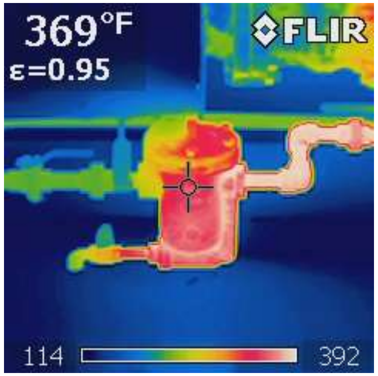
# Steam Traps in the Field

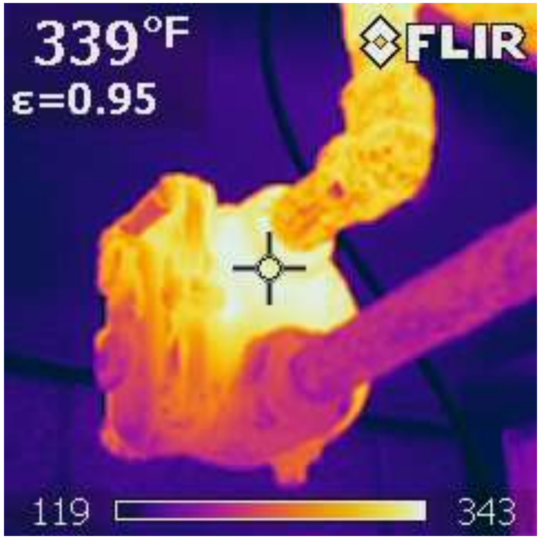


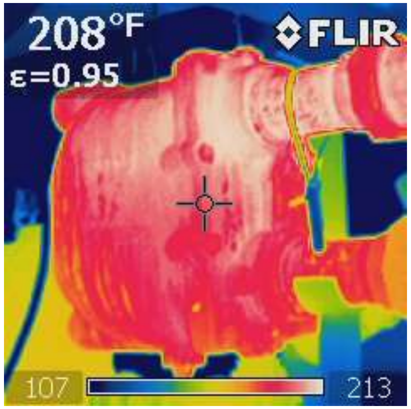



# Steam Trap Failures

- ✓ There have been numerous studies in the industry and one of the more statistically accepted “rule of thumb” is that 10% of traps fail every year
- ✓ This depends on several factors and can be very industry specific also
- ✓ The main failure modes are:
  - Failed closed
  - Failed open
  - Failed partially leaking or partially closed
- ✓ Failed open and failed closed result in the greatest system impacts
  - These failure modes are the most readily recognized
  - These failures should be of first priority

# Steam Trap Investigation for Performance

- ✓ There are several methods for investigating steam trap performance
  - Visual
  - Acoustic
  - Thermal
- ✓ Most times, using only one method maybe inconclusive – so the following is recommended
  - Combination of methods
  - Additional process or system information, is required
- ✓ New state-of-the-art in-trap (real-time) monitoring is available for some steam traps

# Visual Steam Trap Investigation

- ✓ Limited in applicability
  - Most condensate systems are closed
  - Safety and practicality limit the use of this method
- ✓ Individual trap operation and application must be understood
  - Intermittent
  - Continuous
- ✓ Several traps can return condensate via a cascaded condensate return system – condensate receiver vent becomes the point of visual inspection

# Acoustic Steam Trap Investigation

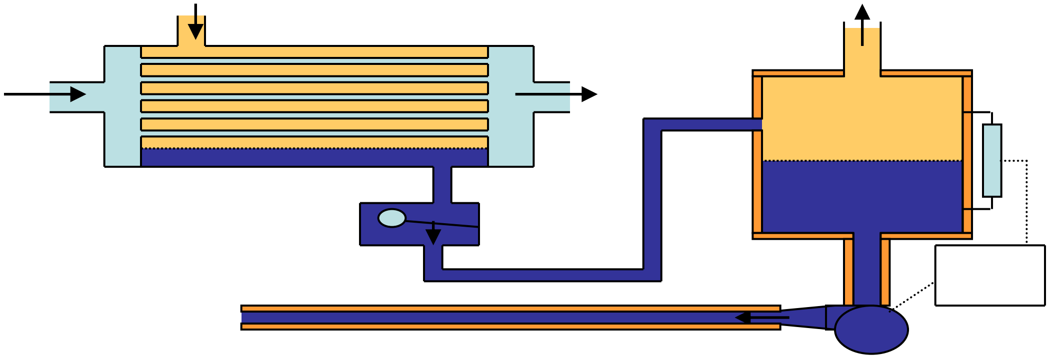
- ✓ Many instruments are available
  - Screw driver
  - Stethoscope
  - Ultrasonic devices
- ✓ Individual trap operation and application must be understood
- ✓ Ultrasonic sensing is typically the most practical
- ✓ Some manufacturers have tools that can take the acoustic signature of steam flow through the trap and use that information to detect failure

# Thermal Steam Trap Investigation

- Many instruments are available
  - Temperature stick
  - Infra-red temperature gun
  - Infra-red thermography camera
- Individual trap operation and application must be understood
- Data can be inconclusive
  - Condensate and steam will take a temperature drop while going through an orifice – hence, difficult to say if trap is failed open!

# Steam Trap Survey - Condensate Recovery Investigation

- ✓ Is condensate being recovered?
- ✓ Is the condensate recovered *to the boilers* with the greatest practical thermal energy?
- ✓ Does the condensate recovery system place excessive backpressure on the traps?
- ✓ Is flash steam recovery applicable?
- ✓ Design the condensate recovery system for the greatest effectiveness



Source: US DOE ITP Steam BestPractices Program

# Steam Trap Installation

- ✓ Each trap must be installed properly
- ✓ Non-condensable gas and startup considerations must be targeted
- ✓ The condensate collection system must be considered
  - Backpressure considerations
  - Lift considerations
  - Two-phase flow considerations

Source: US DOE ITP Steam BestPractices Program

# Effective Steam Trap Management Program

- ✓ Maintain a steam trap database
  - Type of trap, model number, size, etc
  - Application
  - Energy loss if failed open
  - Problems if failed closed
  - When was the last recorded failure, repair
- ✓ Prioritize repairs based on loss estimates and criticality of steam system and production operations
- ✓ Daily monitor receiver vents
- ✓ Inspect all traps at least once a year
- ✓ Trap maintenance training is essential

# Steam Trap Savings Analysis

✓ 1st method

- Use SSAT to predict savings – preliminary estimate
- Number of traps & last maintenance done

✓ 2nd method

- Use SSAT to provide savings
- Number of failed traps

✓ 3rd method

- Use orifice size and calculate steam leak flow
- Use SSAT – Project 1 as demand savings
- Most accurate method – especially for cogeneration systems

# SSAT Project 16 - Savings Analysis

- 1st method (Option 1)
  - Use SSAT to predict savings – preliminary estimate
  - Number of traps & last maintenance done
  - Very GROSS Estimate

**Project 16 - Steam Trap Losses**
Losses calculated from user-defined data

| | |
|---|---|
| Do you wish to model the impact of a maintenance program? | Option 1 - Yes, model to estimate new loss values |

Note: For Option 1, the model estimates a new trap failure rate. The rate reported is for 6 months after the maintenance program is carried out

| | | |
|---|---|---|
| Option 2 - Trap failures on HP header | 5 | Failures > Current - Model will use 0 |
| Option 2 - Trap failures on MP header | 5 | Failures > Current - Model will use 0 |
| Option 2 - Trap failures on LP header | 5 | Failures > Current - Model will use 0 |

Note: Calculated values based on current user inputs are:-
HP header - Trap failures: 0, Loss per trap 0.034 t/h - Total trap loss = 0.00 t/h.
MP header - Trap failures: 0, Loss per trap 0.014 t/h - Total trap loss = 0.00 t/h.
LP header - Trap failures: 0, Loss per trap 0.003 t/h - Total trap loss = 0.00 t/h.

# SSAT Project 16 - Savings Analysis

✓ 2nd method (Option 2)

- Use SSAT to provide savings
- Number of failed traps
- A GROSS estimate

**Project 16 - Steam Trap Losses**

Losses estimated automatically by model - Last maintenance program 3-5 years ago

| | |
|---|---|
| Do you wish to model the impact of a maintenance program? | Option 2 - Yes, enter new number of failed traps |

Note: For Option 1, the model estimates a new trap failure rate. The rate reported is for 6 months after the maintenance program is carried out

| | | |
|---|---|---|
| → **Option 2** - Trap failures on HP header | 5 | ← |
| → **Option 2** - Trap failures on MP header | 5 | ← |
| → **Option 2** - Trap failures on LP header | 5 | ← |

Note: Calculated values based on current user inputs are:-

HP header - Trap failures: 5, Loss per trap 0.034 t/h - Total trap loss = 0.17 t/h.

MP header - Trap failures: 5, Loss per trap 0.014 t/h - Total trap loss = 0.07 t/h.

LP header - Trap failures: 5, Loss per trap 0.003 t/h - Total trap loss = 0.02 t/h.

# SSAT Project 1 - Steam Trap Savings Analysis

- ✓ 3rd Method – most accurate
- ✓ Work with open failed steam traps and prepare a list of traps failed at each pressure level

$$m_{steam} = 0.695 \times A_{orifice} \times P_{steam}$$

**Project 1 - Steam Demand Savings (Changing the process steam requirements)**
Current use - HP: 20 t/h (12273 kW) MP: 40 t/h (26660 kW) LP: 76 t/h (54448 kW)

| | |
|---|---|
| Do you wish to specify steam demand savings? | Yes |

| | | |
|---|---|---|
| If yes, enter HP steam saving | 0 t/h | |
| If yes, enter MP steam saving | 0 t/h | |
| If yes, enter LP steam saving | 0 t/h | |

Note: A negative saving can be entered to model an increase in steam demand

Note: The savings have been converted to heat duties of 0 kW (HP), 0 kW (MP) and 0 kW (LP) based on current header enthalpies

Note: These heat duties are then used to determine the actual flow change in the Projects Model based on the calculated header enthalpies

# Key Points / Action Items

1. *There are different kinds of steam traps and hence, functionality and principles of operation must be understood*
2. *Major steam trap failure modes - open / closed*
3. *An effective steam trap management program must be in place*
4. *There are several commercially available tools for steam trap investigations*
5. *Conduct a steam trap audit at least once a year and repair/replace defective traps*
6. *Steam trap manufacturers are a valuable resource*

# Condensate Recovery

- ✓ Condensate is produced after steam has transferred all its thermal energy and condensed into water
- ✓ Nevertheless, there is significant thermal energy in condensate
- ✓ Every unit of condensate returned implies one less unit of make-up required
- ✓ Returning condensate
  - Reduces energy (steam required) in deaerator
  - Reduces make-up water
  - Reduces chemicals for water treatment
  - Reduces quenching water
  - May reduce blowdown

# Condensate Recovery

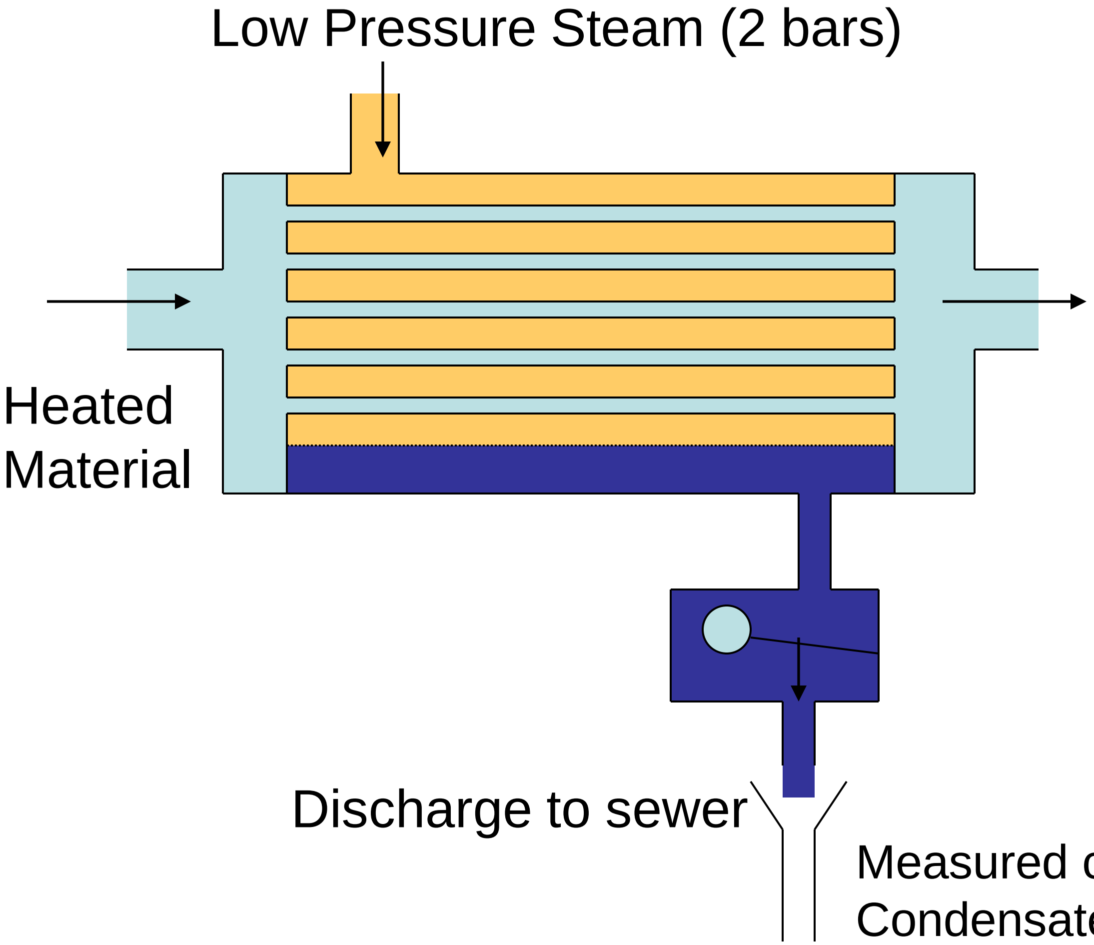
- Condensate typically has worth
  - Energy
  - Make-up water reduction
    - This generally improves feedwater quality
      - Resulting in a reduction in boiler blowdown
  - Chemical
- Condensate recovery costs generally center on the recovery system piping
  - Recovery equipment
  - Return piping

# Condensate Recovery

- ✓ Condensate receivers serving "areas" can reduce project costs
- ✓ Condensate receivers and flash tanks serve to reduce the amount of steam entering the condensate return piping reducing flow restriction problems
- ✓ Contaminated condensate is a critical issue
- ✓ Receiver vents are indicative of trap failures
- ✓ Pump NPSH issues must be investigated

**Source: US DOE ITP Steam BestPractices Program**

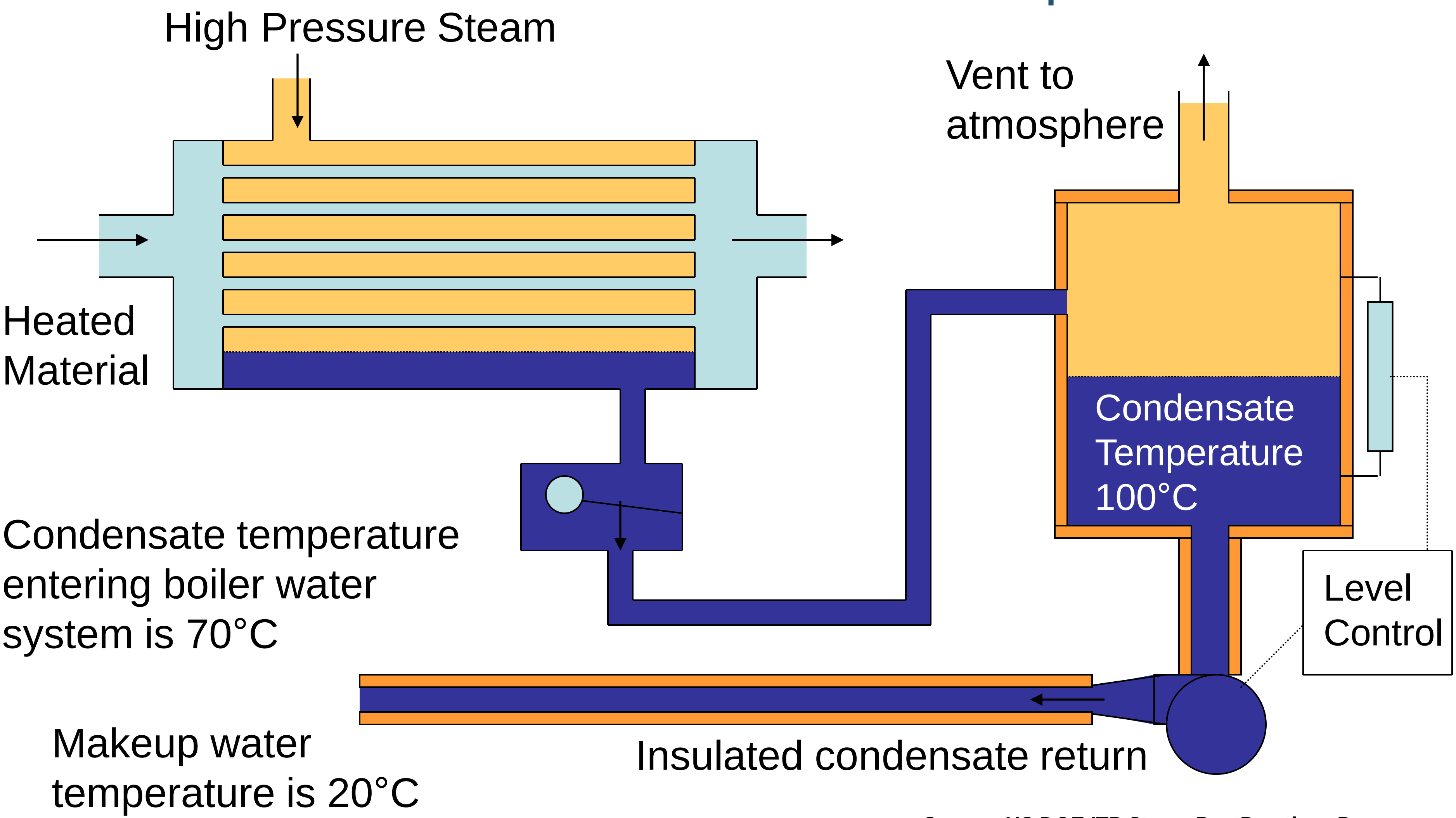
# Condensate Return Example




Measured condensate temperature 100°C. Condensate flow measured by bucket and stopwatch (mass and energy balance is also a common method) to be 50 litres/minute

**Source: US DOE ITP Steam BestPractices Program**

# Condensate Return Example




Source: US DOE ITP Steam BestPractices Program

# Condensate Return Example

- ✓ Enthalpy of condensate: 293.1 kJ/kg
- ✓ Enthalpy of make-up: 83.9 kJ/kg
- ✓ Condensate flow rate: 50 litres/min

} From Steam Tables

$$m_{condensate} = 50 \times 977.8 \times \frac{1}{1000} \times \frac{1}{60} = 0.81 \frac{kg}{s}$$

$$Q_{condensate} = m_{condensate} \times \left(h_{condensate} - h_{makeup}\right)$$

$$Q_{condensate} = 0.81 \times (293.1 - 83.9) = 169.5\, kW$$

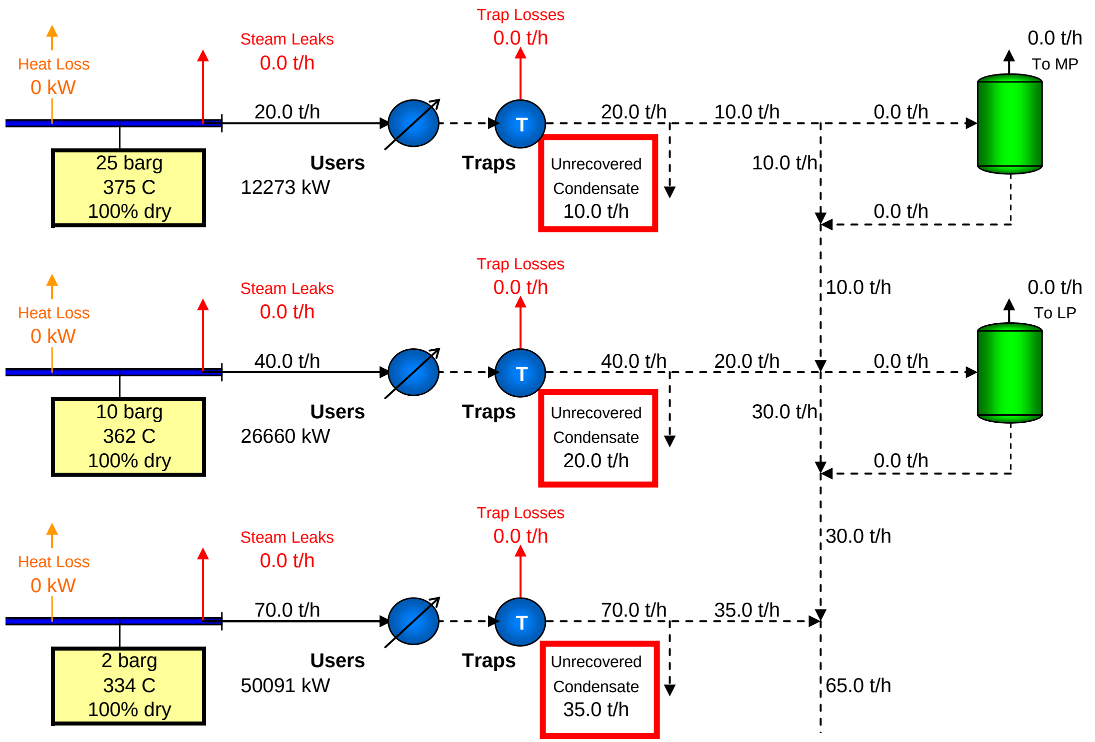
$$Q_{system} = Q_{condensate} \times \frac{1}{\eta_{boiler}} = 169.5 \times \frac{1}{0.80} = 212\, kW$$

$$Energy\ Savings = 212 \times 3{,}600 \times \frac{1}{40{,}144} \times 0.52 \times 8{,}760 \approx \$87{,}000$$

# SSAT Project 13 - Condensate Return Savings

| Process Condensate | Input Data | Warnings |
|---|---|---|
| Condensate return temperature to tank | 70 °C | |
| HP condensate recovery | 50 % | |
| MP condensate recovery | 50 % | |
| LP condensate recovery | 50 % | |

Note: Condensate recovery specified as the percentage of steam supplied to the processes at each level



# SSAT Project 13 – Condensate Return Savings

- ✓ Note that SSAT requires condensate return input as a percent of steam supplied to the process at each header level
  - Manual calculations will be needed to get to the new value of condensate returned
    - Steam demand on LP = 76 Tph
    - Current condensate returned = 50%
    - Current condensate returned = 35 Tph
    - Additional condensate = 0.81 kg/s = 2.92 Tph
    - New condensate return = 35 + 2.92 = 37.92 Tph
    - New condensate return = 37.92 / 70 = 54.17%

# SSAT Project 13 – Condensate Return Savings

| Project 13 - Condensate Recovery<br>Currently recover 50% of HP, 50% of MP and 50% of LP at 70°C |
|---|

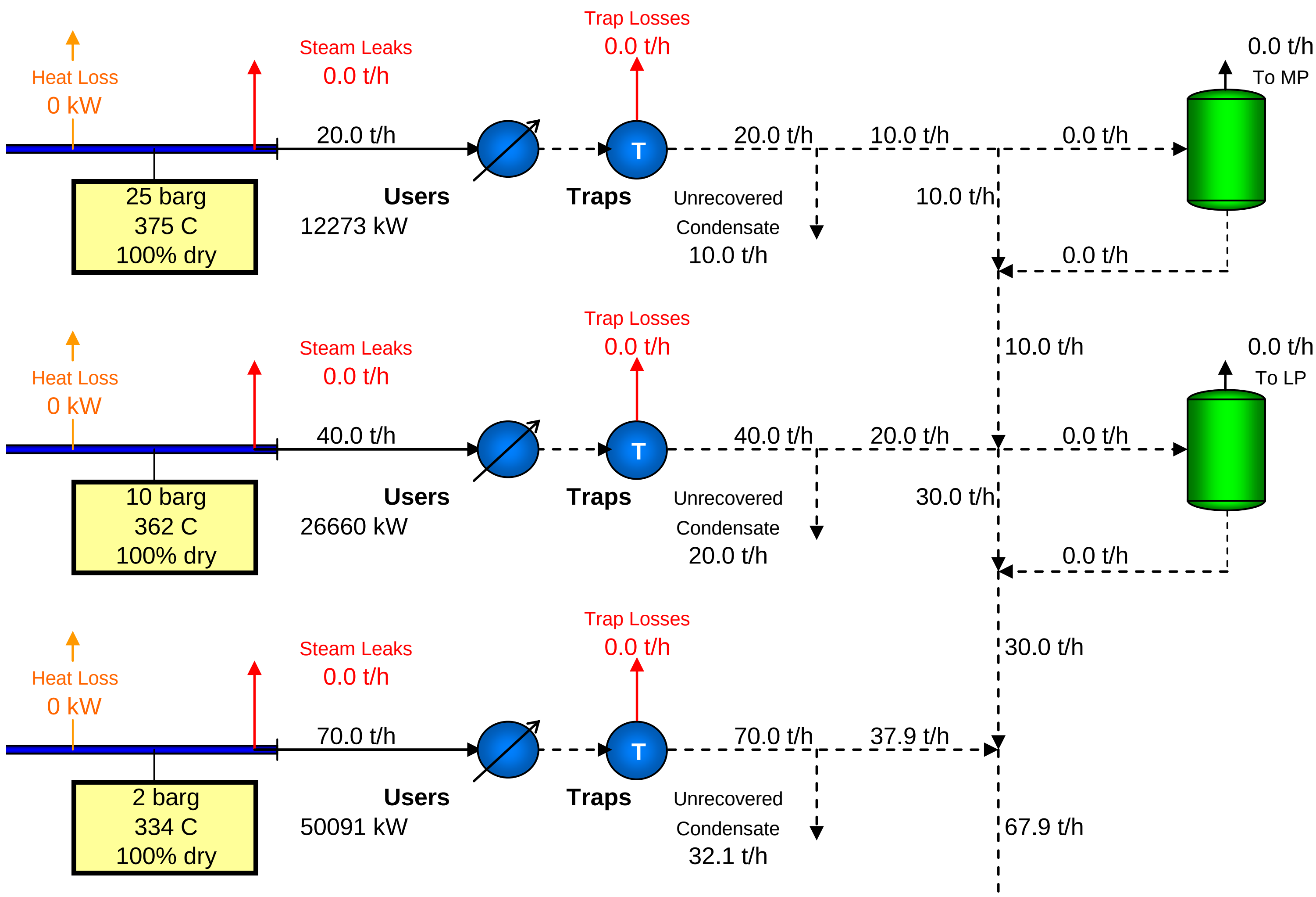
| Do you wish to specify new condensate recovery rates? | Yes |
|---|---|

| | | |
|---|---|---|
| → If yes, enter new HP condensate recovery | 50 | % ← |
| → If yes, enter new MP condensate recovery | 50 | % ← |
| → If yes, enter new LP condensate recovery | 54.17 | % ← |

Note: Condensate return temperature will be assumed to be 70°C as for the current operation

- ✓ Note that SSAT needs information of condensate recovery on all the headers even though the project being modeled is only on one of the headers
  - Other headers should have the same numbers as the "Input" page

# SSAT Project 13 – Condensate Return Savings



# SSAT Project 13 – Condensate Return Savings

## Results Summary

### SSAT Default 3 Header Metric Model Moldova Ex 5

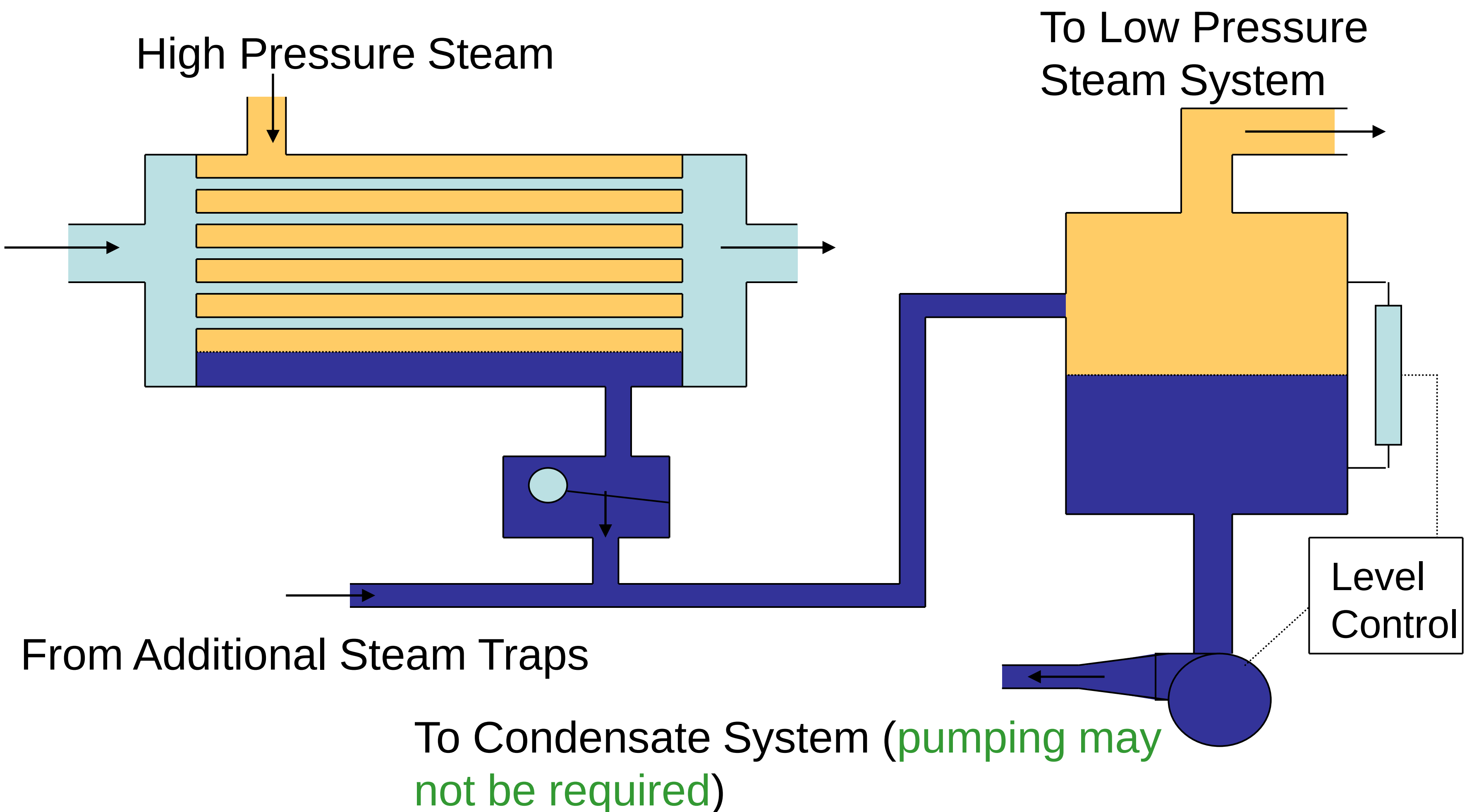
*Model Status : OK*

| Cost Summary ($ '000s/yr) | Current Operation | After Projects | Reduction | |
|---|---|---|---|---|
| Power Cost | 6,132 | 6,132 | 0 | 0.0% |
| Fuel Cost | 55,289 | 55,206 | 83 | 0.1% |
| Make-Up Water Cost | 1,086 | 1,042 | 44 | 4.0% |
| **Total Cost (in $ '000s/yr)** | **62,507** | **62,380** | **126** | **0.2%** |

| On-Site Emissions | Current Operation | After Projects | Reduction | |
|---|---|---|---|---|
| CO2 Emissions | 221739 t/yr | 221408 t/yr | 332 t/yr | 0.1% |
| SOx Emissions | 0 t/yr | 0 t/yr | 0 t/yr | N/A |
| NOx Emissions | 439 t/yr | 438 t/yr | 1 t/yr | 0.1% |

| Utility Balance | Current Operation | After Projects | Reduction | |
|---|---|---|---|---|
| Power Generation | 2000 kW | 2000 kW | - | - |
| Power Import | 5000 kW | 5000 kW | 0 kW | 0.0% |
| Total Site Electrical Demand | 7000 kW | 7000 kW | - | - |
| Boiler Duty | 140763 kW | 140552 kW | 211 kW | 0.1% |
| Fuel Type | Natural Gas | Natural Gas | - | - |
| Fuel Consumption | 12623.1 Nm3/h | 12604.2 Nm3/h | 18.9 Nm3/h | 0.1% |
| Boiler Steam Flow | 150.1 t/h | 149.9 t/h | 0.2 t/h | 0.1% |
| Fuel Cost (in $/MWh) | 44.84 | 44.84 | - | - |
| Power Cost (as $/MWh) | 140.00 | 140.00 | - | - |
| Make-Up Water Flow | 73 m3/h | 70 m3/h | 3 m3/h | 4.0% |

# Cascade Condensate Systems




Source: US DOE ITP Steam BestPractices Program

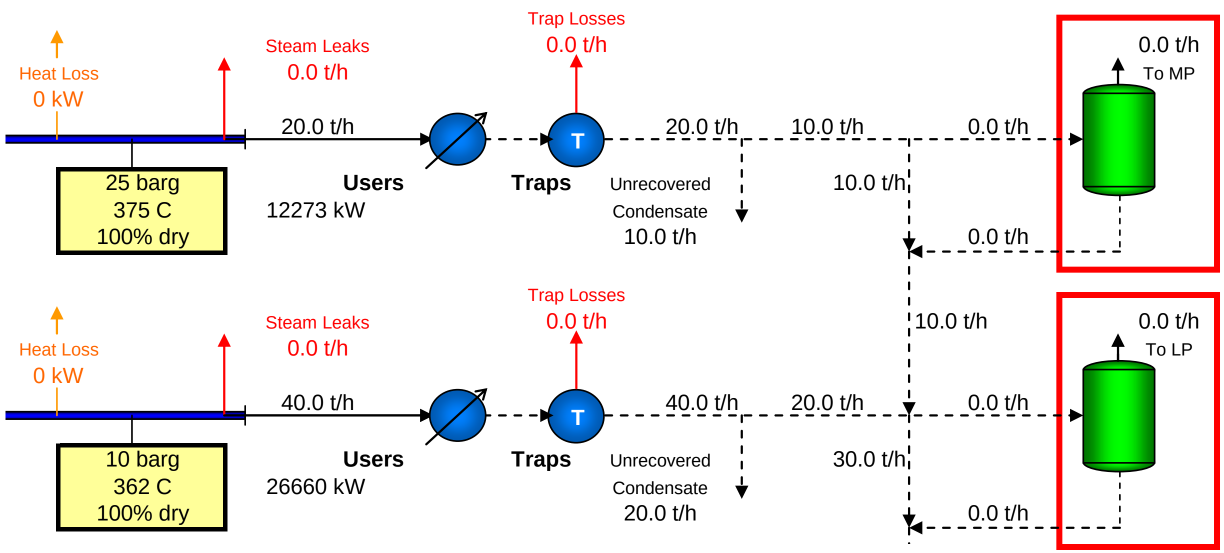
# SSAT Projects 14 & 15 - Condensate Flash Tanks

**Project 14 - Condensate Flash to MP**
Not currently installed

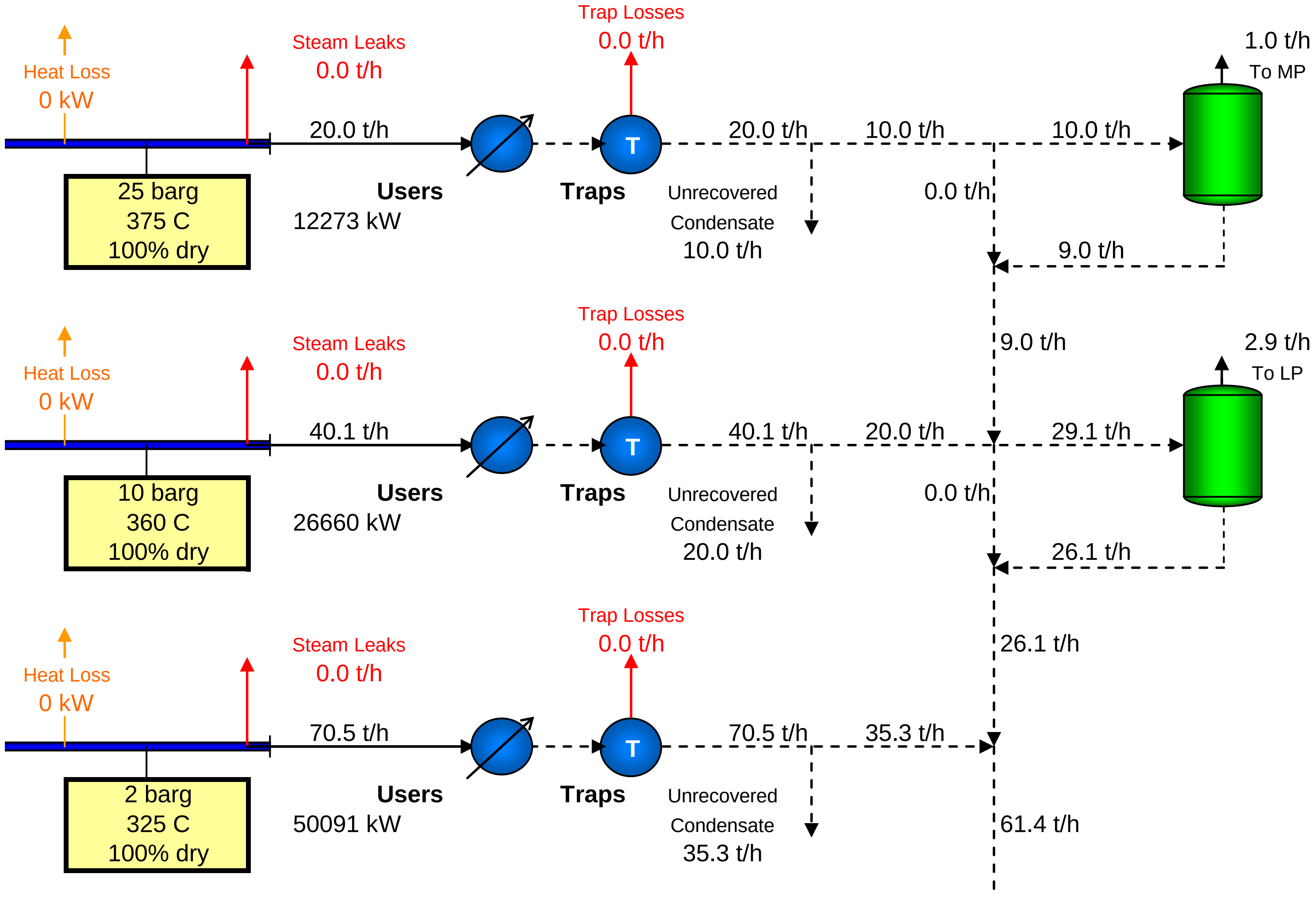
| | |
|---|---|
| Do you wish to modify the MP condensate flash system? | Yes, install condensate flash to MP |

**Project 15 - Condensate Flash to LP**
Not currently installed

| | |
|---|---|
| Do you wish to modify the LP condensate flash system? | Yes, install condensate flash to LP |



# SSAT Projects 14 & 15 – Condensate Flash Tanks



# SSAT Project 14 & 15 – Condensate Flash Tanks

## Results Summary

### SSAT Default 3 Header Metric Model Moldova Ex 7

*Model Status : OK*

| Cost Summary ($ '000s/yr) | Current Operation | After Projects | Reduction | |
|---|---|---|---|---|
| Power Cost | 6,132 | 6,132 | 0 | 0.0% |
| Fuel Cost | 55,289 | 54,024 | 1,265 | 2.3% |
| Make-Up Water Cost | 1,086 | 1,087 | -2 | -0.1% |
| **Total Cost (in $ '000s/yr)** | **62,507** | **61,243** | **1,264** | **2.0%** |

| On-Site Emissions | Current Operation | After Projects | Reduction | |
|---|---|---|---|---|
| CO2 Emissions | 221739 t/yr | 216665 t/yr | 5075 t/yr | 2.3% |
| SOx Emissions | 0 t/yr | 0 t/yr | 0 t/yr | N/A |
| NOx Emissions | 439 t/yr | 429 t/yr | 10 t/yr | 2.3% |

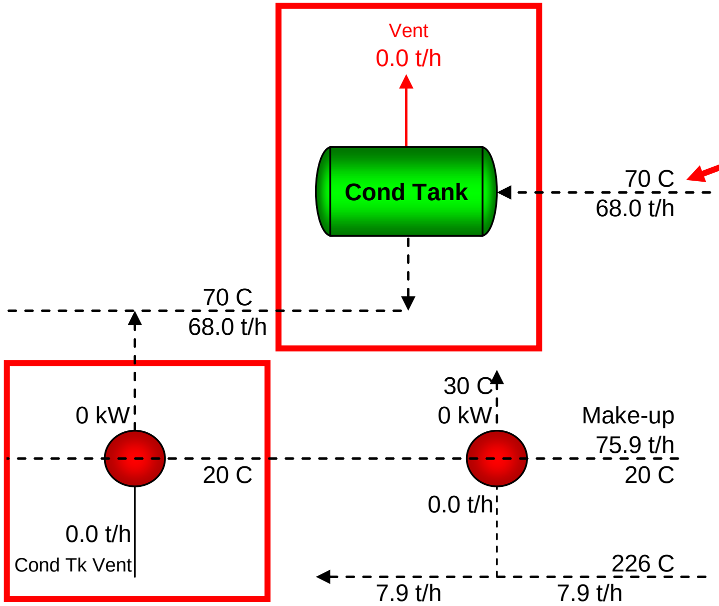
| Utility Balance | Current Operation | After Projects | Reduction | |
|---|---|---|---|---|
| Power Generation | 2000 kW | 2000 kW | - | - |
| Power Import | 5000 kW | 5000 kW | 0 kW | 0.0% |
| Total Site Electrical Demand | 7000 kW | 7000 kW | - | - |
| | | | | |
| Boiler Duty | 140763 kW | 137542 kW | 3221 kW | 2.3% |
| Fuel Type | Natural Gas | Natural Gas | - | - |
| Fuel Consumption | 12623.1 Nm3/h | 12334.2 Nm3/h | 288.9 Nm3/h | 2.3% |
| Boiler Steam Flow | 150.1 t/h | 146.7 t/h | 3.4 t/h | 2.3% |
| | | | | |
| Fuel Cost (in $/MWh) | 44.84 | 44.84 | - | - |
| Power Cost (as $/MWh) | 140.00 | 140.00 | - | - |
| | | | | |
| Make-Up Water Flow | 73 m3/h | 73 m3/h | 0 m3/h | -0.1% |

# SSAT Project 11 – Condensate Tank Vent HX

| Project 11 - Feedwater Heat Recovery Exchanger using Condensate Tank Vent |
|---|
| Not currently installed |

| Modify the condensate tank vent heat recovery system? | No |
|---|---|

Note: An approach temperature of 10°C will be assumed for a new exchanger




Condensate return Temperature should be > 100°C

- ✓ Note that this Project is possible ONLY with condensate return temperatures > 100°C

# Key Points / Action Items

1. Returning condensate
   - Reduces energy
   - Reduces make-up water
   - Reduces chemicals for water treatment
   - Reduces quenching water
   - May reduce blowdown
2. Condensate recovery is often neglected but it can provide significant energy savings
3. Quantify the amount of condensate being recovered in a plant using a simple mass balance on the entire steam system
4. Identify potential areas of condensate recovery

# Common BestPractices - Recovery

- ✓ Implement an effective steam-trap management and maintenance program
- ✓ Recover as much as possible of available condensate
- ✓ Recover condensate at the highest possible thermal energy
- ✓ Flash high-pressure condensate to make low-pressure steam

Source: US DOE BestPractices Steam System Sourcebook